

How to select Heat Exchanger

You can select heat exchanger simply by the catalog. Please refer to the following instruction.

STEP.1 Working condition check

Check item	Remarks
Type	Water-Cooled Shell and Tube type, Air-Cooled type
Heat exchange amount	If not specified, temperature of inlet and outlet at shell side should be set.
Working temperature	Shell side: inlet and outlet temperature Tube side: inlet temperature
Max working pressure	1 MPa for both Shell and Tube type and Air-Cooled type
Flow rate (normal/max)	Shell side: Should be specified Tube side: If not specified, set the same value as a shell side.

Heat exchanger selection is NOT possible if check item in **large character** is not specified.

Check item	Remarks
Fluid type	Shell side: Fluid type, density, and kinematic viscosity Tube side: Type of cooling water
Allowable pressure drop	If not specified, Shell side: $\leq 0.1\text{MPa}$ Tube side: $\leq 0.05\text{MPa}$
Scale coefficient	If not specified, set $0\text{ m}^2\text{C/W}$ for both shell side and tube side.
Pipe connection	Size and connection type (flange/thread) should be specified.

(Standard working condition in the catalog) Fluid: Corresponding to ISO VG46 / Inlet temperature at shell side: 55°C / Inlet temperature at tube side: 30°C

STEP.2 Calculation of required condition

- A) If working condition checked at **STEP 1** is almost same with standard condition in the catalog Go to **STEP.2-①**
- B) If working condition checked at **STEP 1** is NOT same with standard condition in the catalog Go to **STEP.6**

① Calculation of heat transfer area

i) Calculation of heat exchange amount [kW]
(ρ : specific gravity, C: specific heat)
Calculate working temperature by the following equation if heat exchange amount and oil flow rate is determined.

$$Q = W_o \times 60 \times \rho_o \times C_o \times (T_1 - T_2) \\ = W_w \times 60 \times \rho_w \times C_w \times (t_2 - t_1)$$

ii) Calculation of logarithmic mean temperature difference θ [°C]

$$\theta = \frac{(T_1 - t_2) - (T_2 - t_1)}{2.3 \log \frac{(T_1 - t_2)}{(T_2 - t_1)}}$$

iii) Calculation of required heat transfer area A [m²]
(K-value: Overall heat transfer coefficient [W/m²C])

$$A = \frac{Q \times 1000}{\theta \cdot K}$$

Fig.1 Although K-value depends on working condition, structure of heat exchanger, and so on, please select mean value of catalog products.

Type of cooling tube	K - Value
Products of $\phi 9$ low fin tube	350~450
Products of $\phi 12.7$ low fin tube	200~250

[W: Flow rate (ℓ / min), T1/T2: Inlet and outlet temperature at shell side (°C), t1/t2: Inlet and outlet temperature at tube side (°C)]

STEP.3 Base model selection

- ① Select a base model from P.8 - 9 "INDEX" that meets the requirements in **STEP 2**.
- ② Refer to the production line-up page of the selected base model.

TYPE	STRUCTURE	COOLING TUBE	MAX WORKING PRESSURE [MPa]	MODEL	HEAT TRANSFER AREA [m ²]	HEAT EXCHANGE AMOUNT [kW]	SHELL SIDE (OIL) FLOW RATE [ℓ / min]	SPEC. EQUIPMENT, OPTION	PAGE
	Shell tube sheet type 2 pass	Shell Low Fin tube Phosphor-bronze	1.0	FCF	0.01~0.2	0.1~10	10~100		
				TCC	0.1~1	1~10	10~100		
				ZCC	1.0~10	10~100	10~100		

STEP.4 Size selection

Refer to "PERFORMANCE GRAPH" of the selected model in **STEP 3**, and select the minimum size within the determined condition of heat exchange amount and allowable pressure drop.

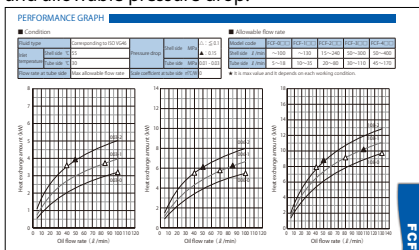


Fig.2 Oil quantity variation

Oil flow rate	Large	Small
CODE	0	1 2

Fig.3 How to check heat transfer area of heat exchanger

Type	How to check
FCF*1, FCD(B), FCX, FCW, FCU	Divide the last two numbers of MODEL CODE by 20
FCF*2, FPD	Divide the last two numbers of MODEL CODE by 2
FTC(B), FTS(B), TEMA	The number right after MODEL CODE (It is directly heat transfer area.)

(Ex.) In case of FCF-114-2 ==> $14 \div 20 = 0.7\text{m}^2$

* 1 FCF-003~FCF-390 * 2 FCF-311~FCF-420

STEP.5 Spec confirmation

○ Estimate K-value by back calculating in **STEP 2 - ①**, and confirm if the heat transfer area of selected model in **STEP 4** satisfies required specification.

- a) Estimated K-value equals to the one in **fig.1** ⇒ ○ Selected model is OK.
- b) Estimated K-value does not equal to the one in **fig.1** ⇒ × Back to **STEP 4** and select again.

STEP.6 Model selection for other conditions

○ If standard working condition on the catalog does not meet your requirement or if you request air-cooled type heat exchanger, please fill out necessary items from "Request (Filter/Heat Exchanger)" on our WEB site.

Download of drawing, CAD data (outline drawing), and operation manual is available on our WEB site*.

* User account registration is required (for free). https://www.taiseikogyo.co.jp/en/request_cooler/

PERFORMANCE GRAPH

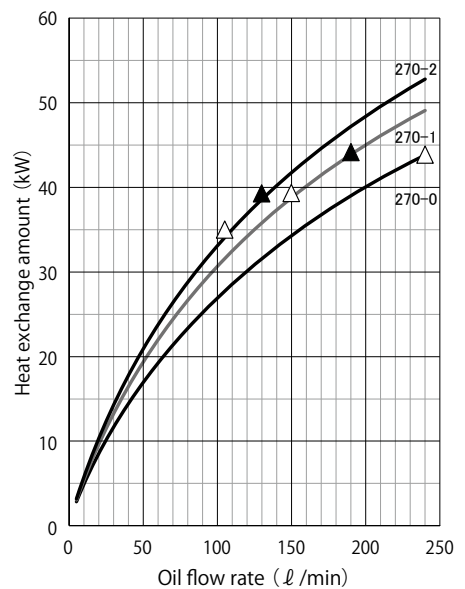
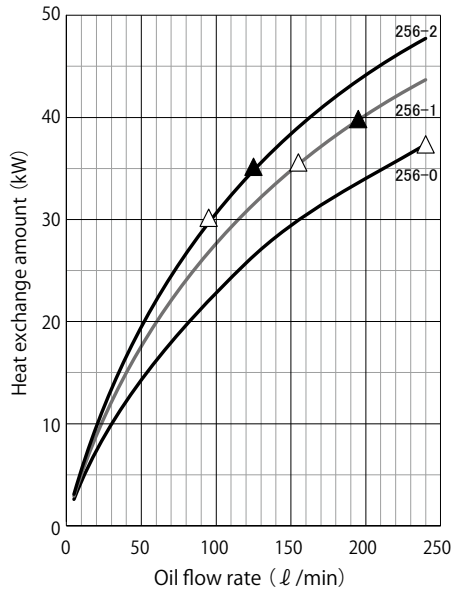
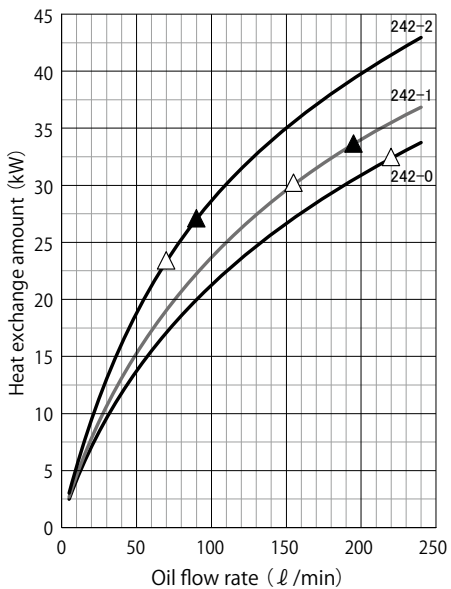
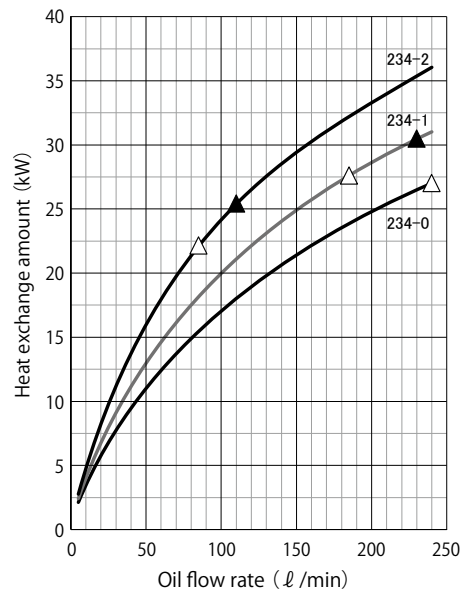
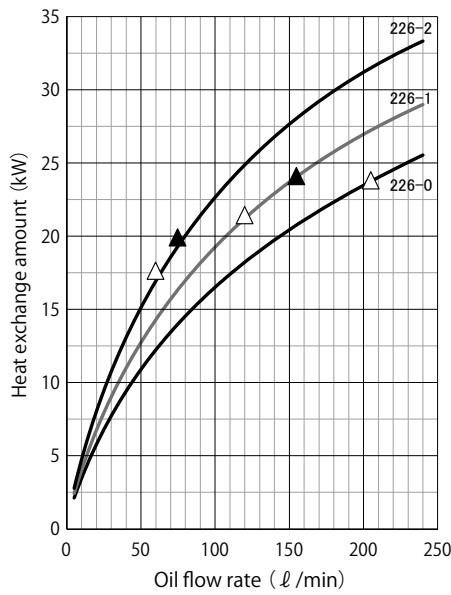
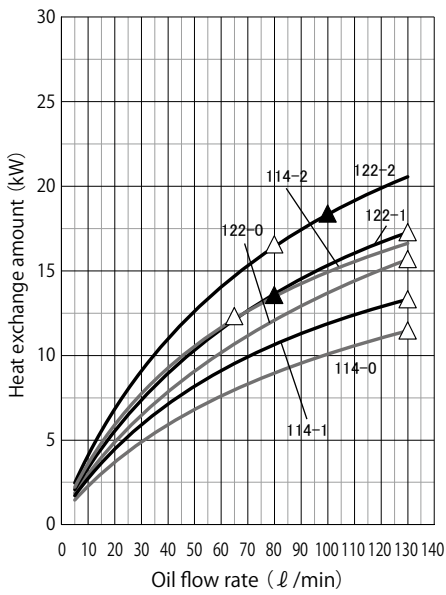
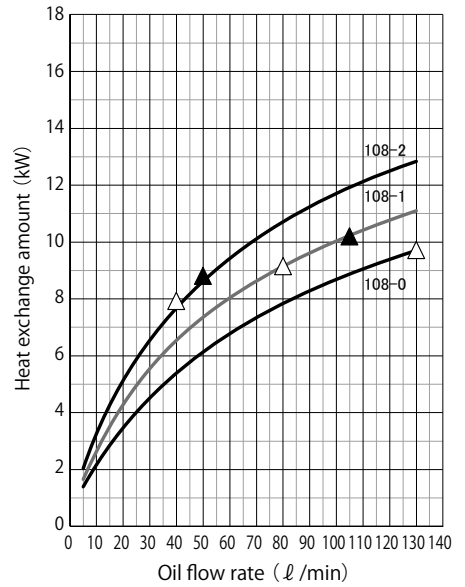
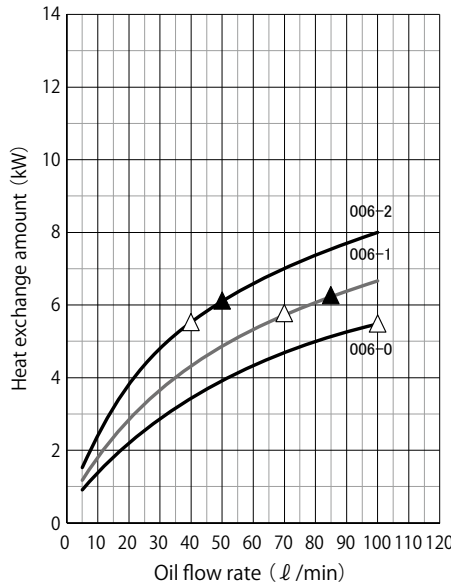
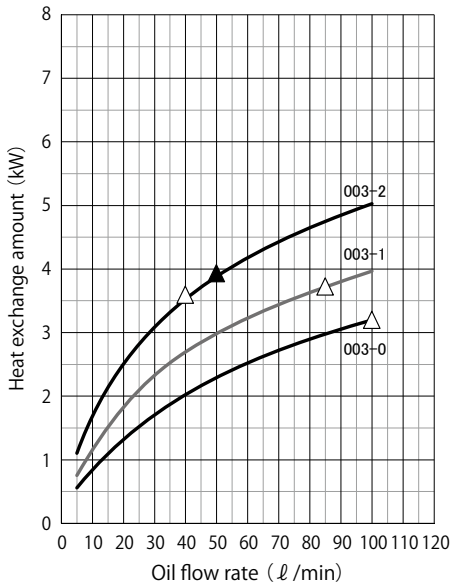
Condition

Fluid type		Corresponding to ISO VG46		Pressure drop	Shell side MPa	Δ : ≤ 0.1
Inlet temperature	Shell side $^{\circ}\text{C}$	55			Tube side MPa	\blacktriangle : 0.15
	Tube side $^{\circ}\text{C}$	30			0.01 - 0.03	
Flow rate at tube side		Max allowable flow rate		Scale coefficient at tube side $\text{m}^2\text{C/W}$		0

Allowable flow rate

Model code	FCF-0□□	FCF-1□□	FCF-2□□	FCF-3□□	FCF-4□□
Shell side ℓ/min	~ 100	~ 130	15 \sim 240	50 \sim 300	50 \sim 400
Tube side ℓ/min	5 \sim 18	10 \sim 35	20 \sim 80	30 \sim 110	45 \sim 170

★ It is max value and It depends on each working condition.



PERFORMANCE GRAPH

■ Condition

Fluid type		Corresponding to ISO VG46		Pressure drop	Shell side MPa	△ : ≤ 0.1
Inlet temperature	Shell side °C	55			Tube side MPa	▲ : 0.15
	Tube side °C	30		Scale coefficient at tube side m ² C/W 0		
Flow rate at tube side		Max allowable flow rate				

■ Allowable flow rate

Model code	FCF-0 □	FCF-1 □	FCF-2 □	FCF-3 □	FCF-4 □
Shell side ℓ/min	~ 100	~ 130	15 ~ 240	50 ~ 300	50 ~ 400
Tube side ℓ/min	5 ~ 18	10 ~ 35	20 ~ 80	30 ~ 110	45 ~ 170

★ It is max value and it depends on each working condition.

